



SWISS QUALITY

DEPTH FILTRATION FOR VALUABLE LIQUIDS. SINCE 1938.

NEW APPROACH FOR SINGLE-USE CLARIFICATION OF BIOLOGICAL SOLUTIONS

LEVITRONIX CONFERENCE JUNE 2022

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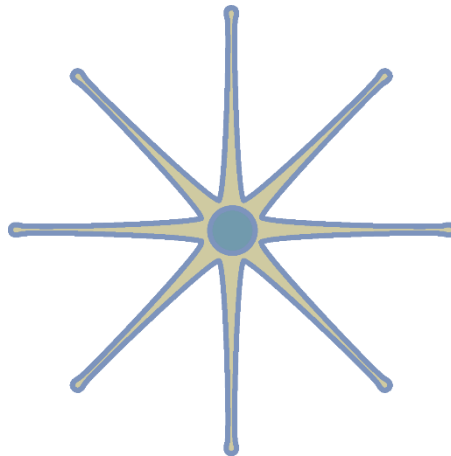
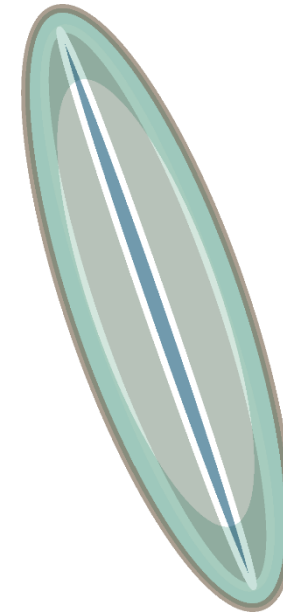
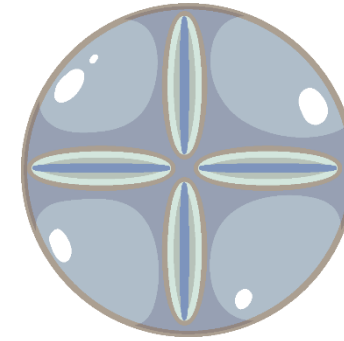
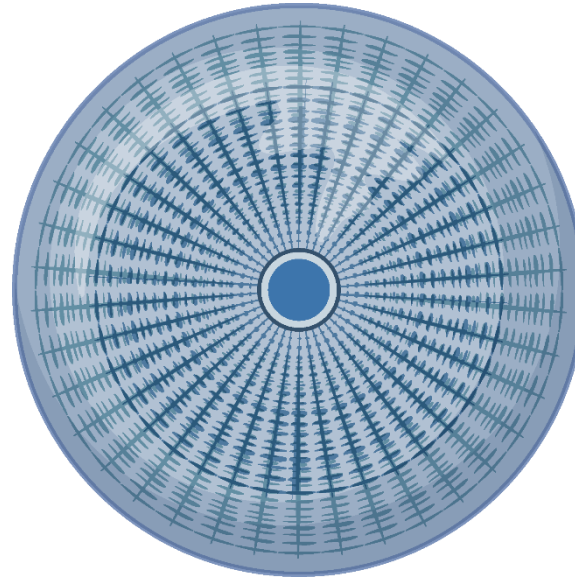
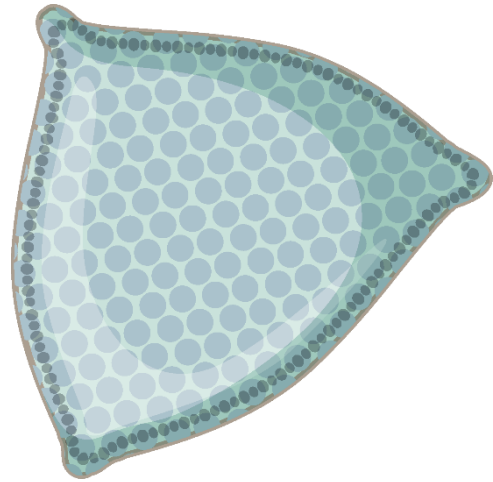
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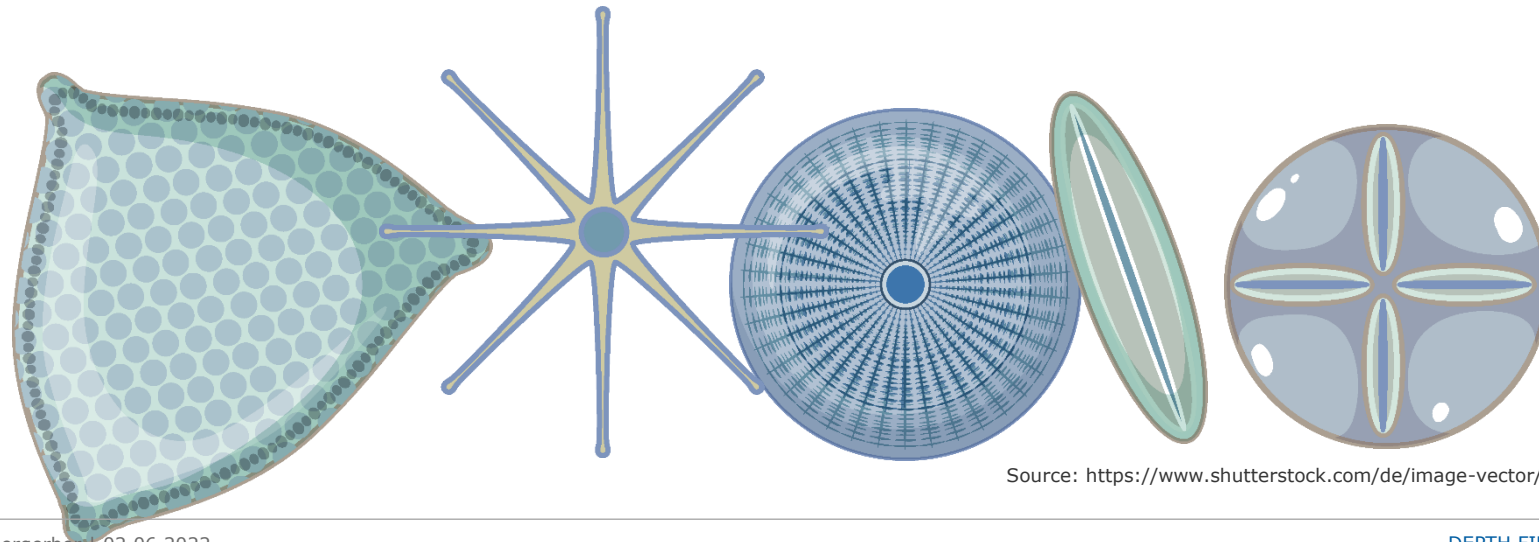


ONCE UPON A TIME...



Source: <https://www.shutterstock.com/de/image-vector/diatom-icons-set-isolated-on-white-1938269887>

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AGENDA



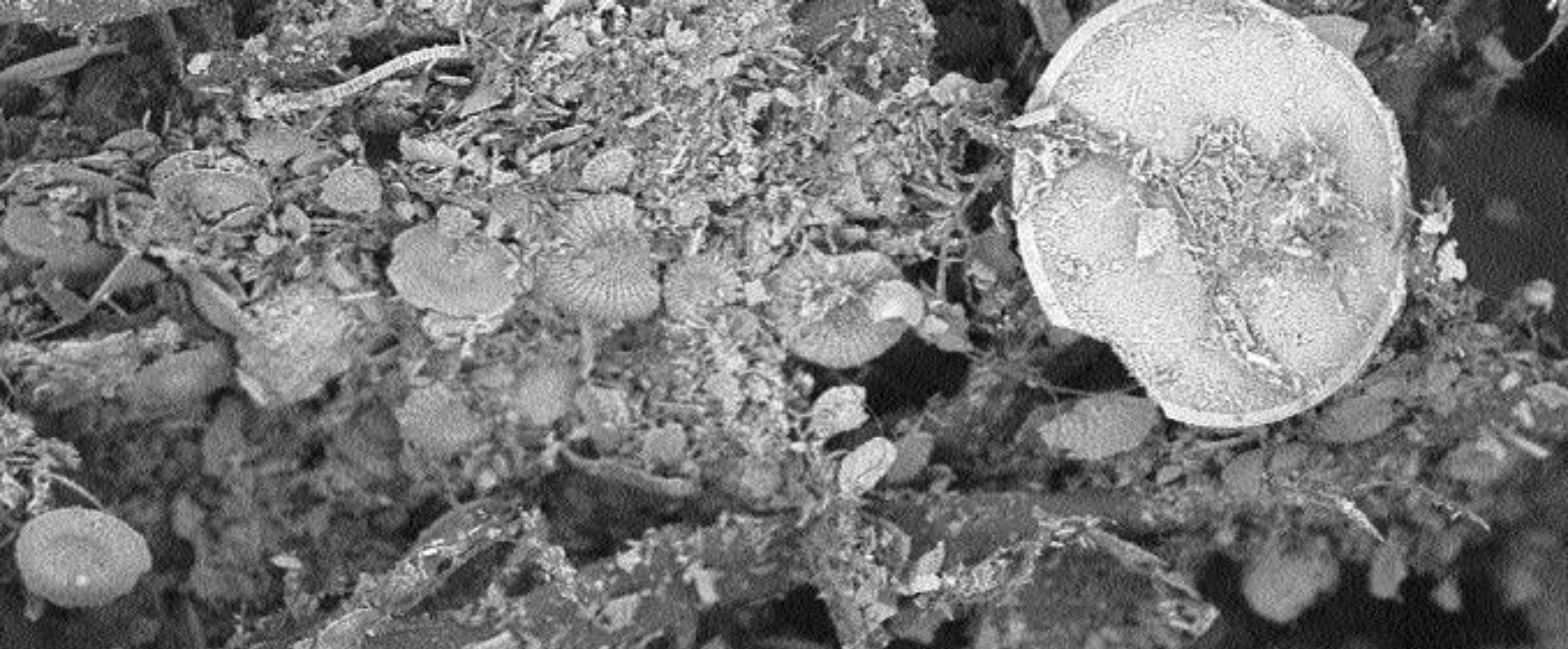
Basics of depth and alluvial filtration

- Trends & Technologies in biomanufacturing
- Sheet vs. Depth vs. Alluvial filtration

Case Studies

- 1) Mammalian Cell removal
- 2) Plasmid DNA clarification
- 3) Depth Filtration vs. Alluvial filtration vs. pH adjustment
- 4) Influence of different filter sheet types
- 5) Scale up

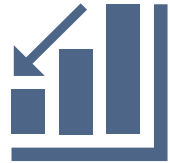
BASICS OF DEPTH FILTRATION



Source: FILTROX AG, 2008

TRENDS

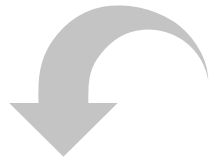
Development and challenges in Biomanufacturing



Reduction of process steps



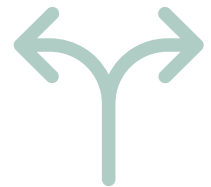
Removal of impurities



Cost reduction



Fast and reliable

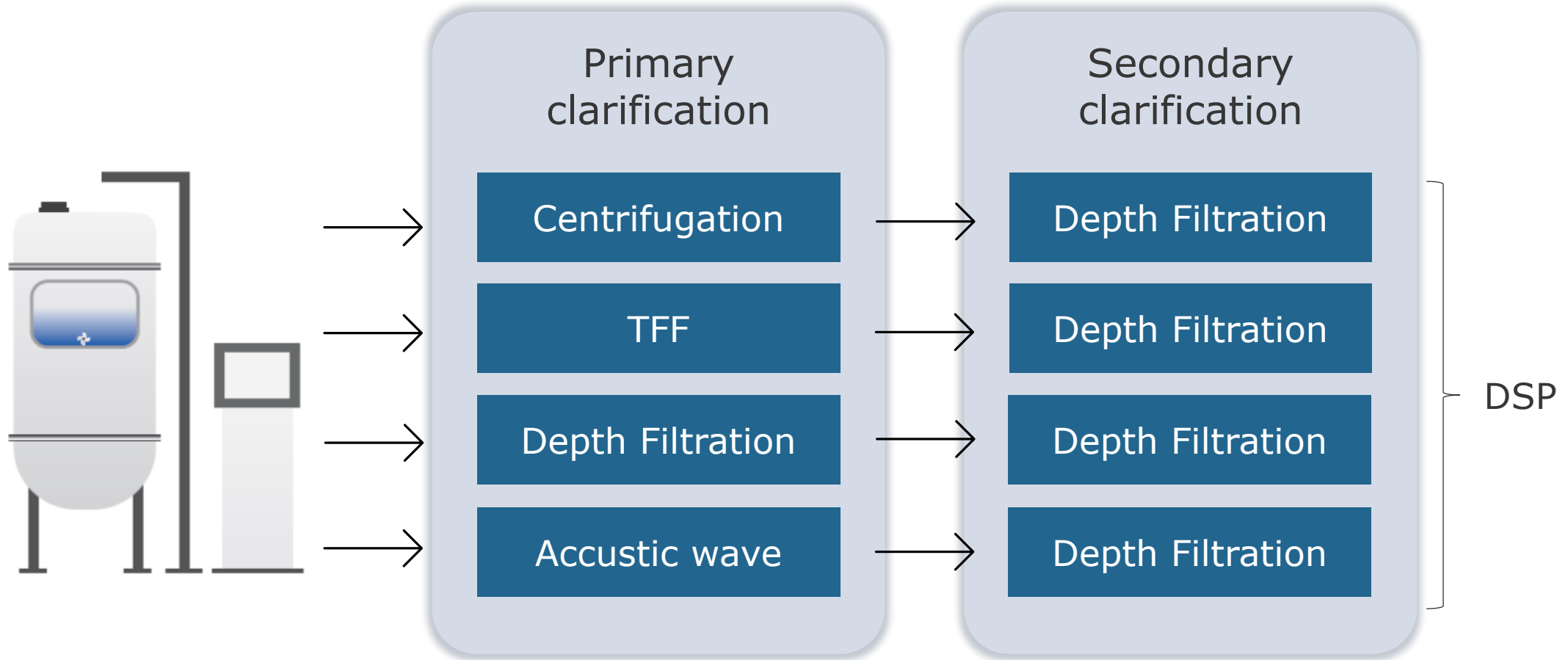


Robust and flexible technology

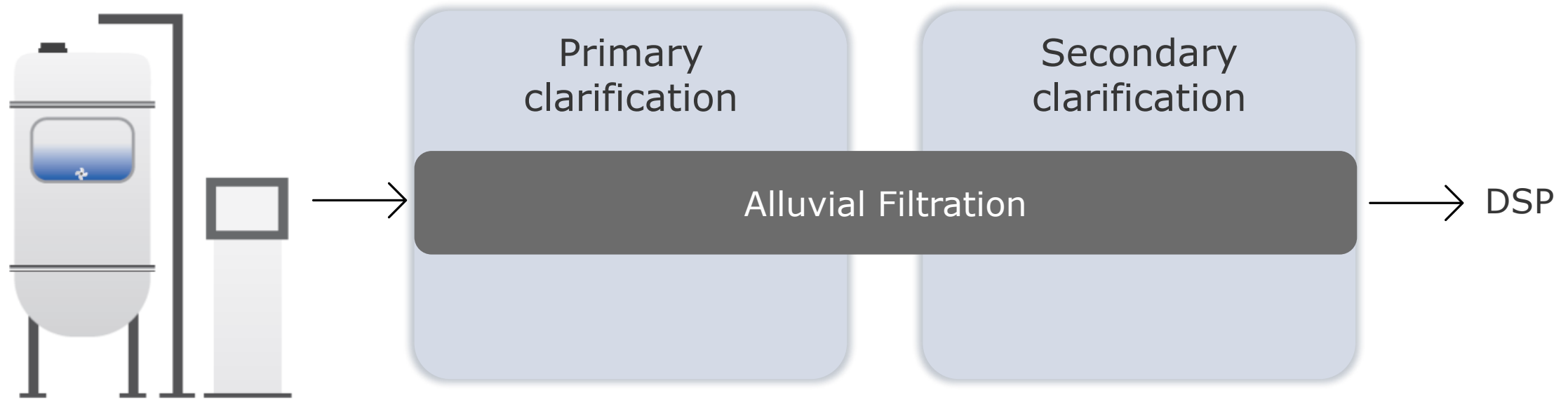


Easy scalable and duplicatable

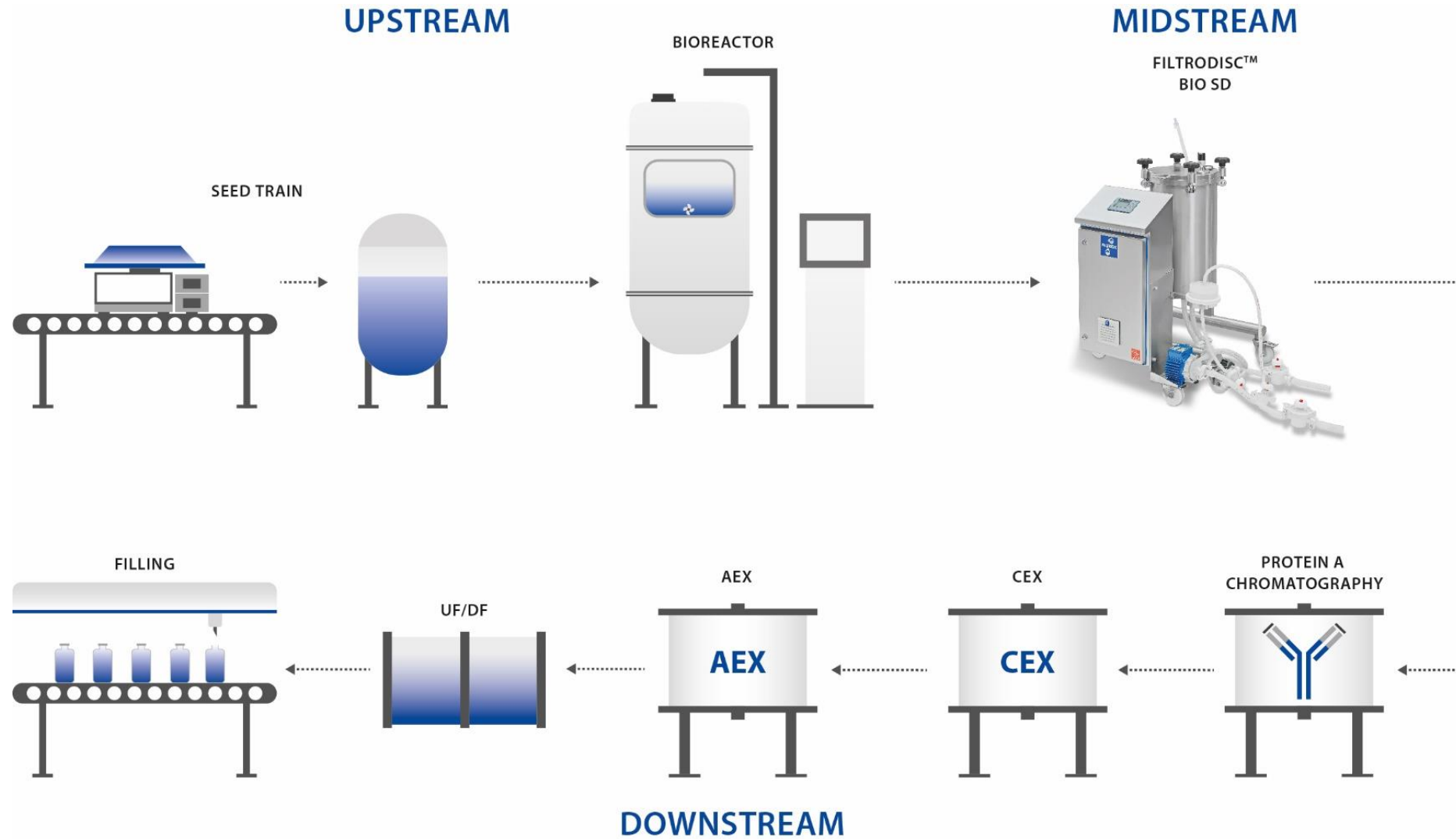
TECHNOLOGY COMPARISON



TECHNOLOGY COMPARISON

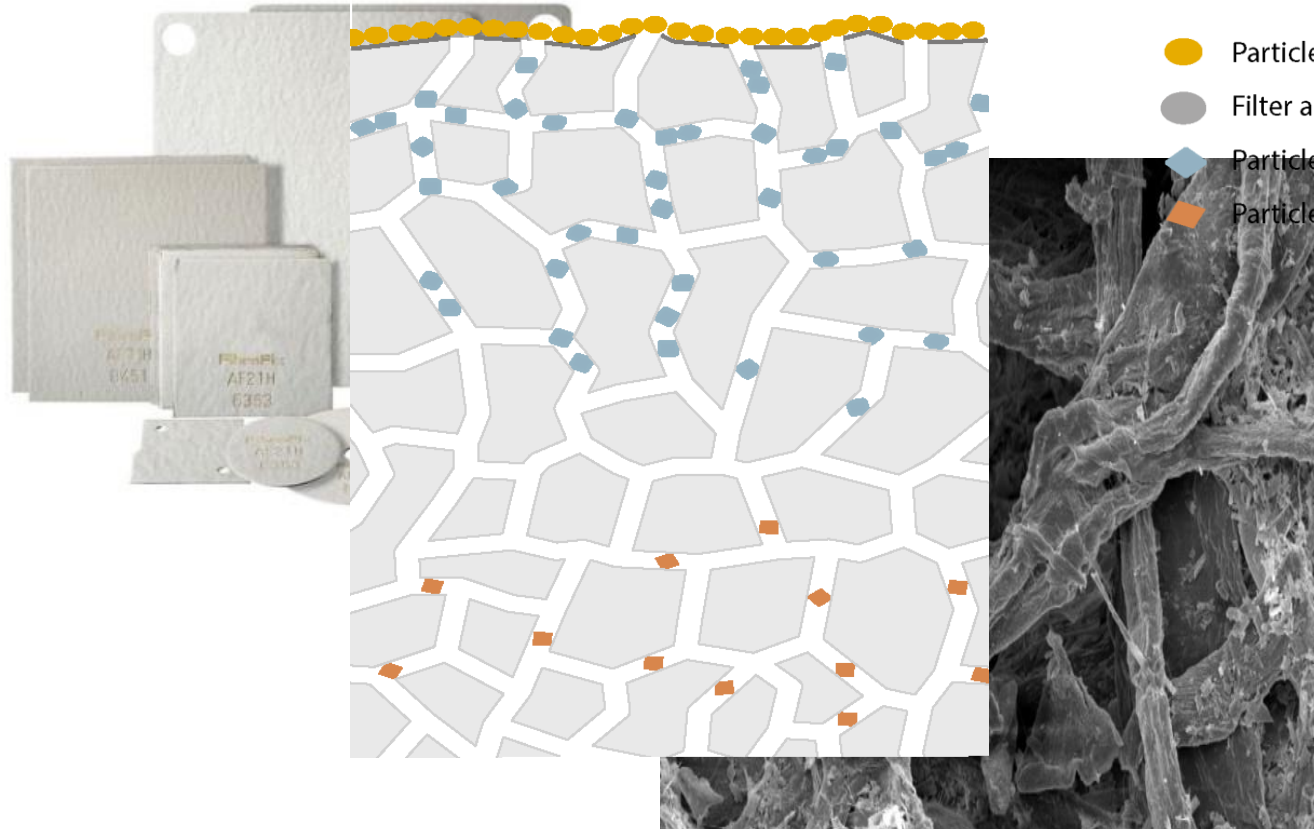


TECHNOLOGY COMPARISON



DEPTH VS. ALLUVIAL FILTRATION

Depth Filtration



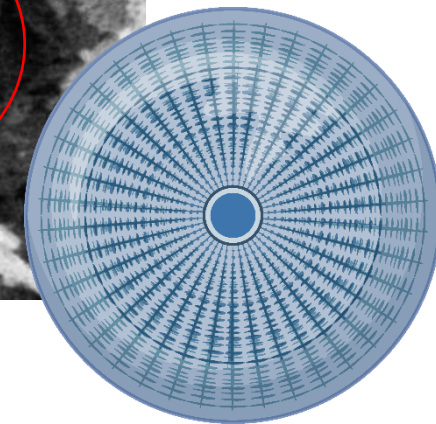
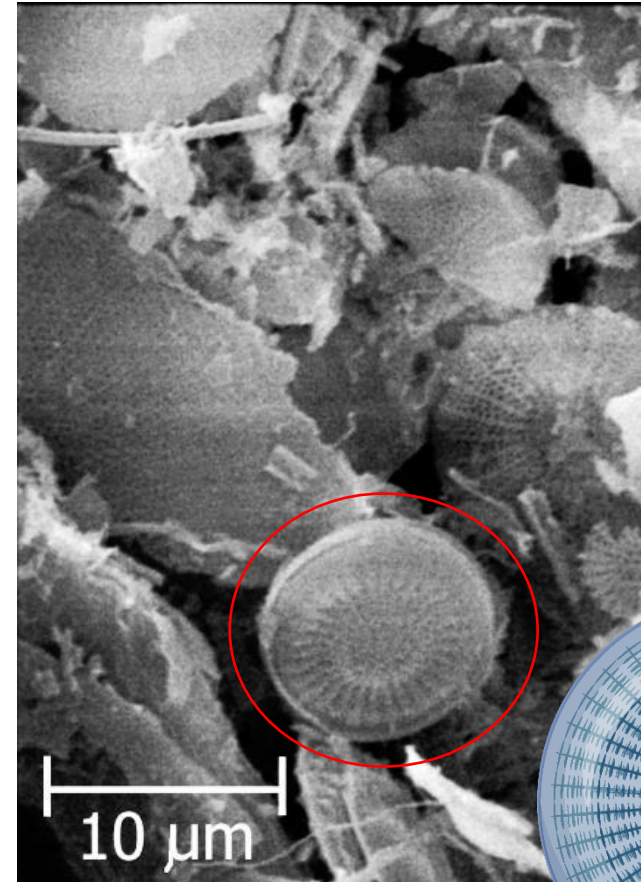
- Particles $> 5 \mu\text{m}$
- Filter aid $> 10 \mu\text{m}$
- ◆ Particles $< 5 \mu\text{m}$
- ◆ Particles $< 1 \mu\text{m}$

Alluvial Filtration



ALLUVIAL FILTRATION

- Large Capacity for high particle load
 - An established technology in pharmaceutical filtration since decades (e. g. plasma fractionation)
 - Long term experience (over 60 years in beer filtration)
 - Filtration through 3D Network
 - Economical
- **Constantly renewed filter surface**

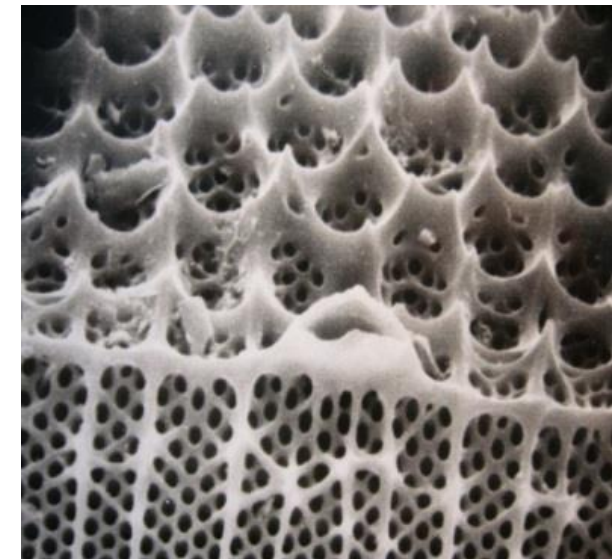


ALLUVIAL FILTRATION

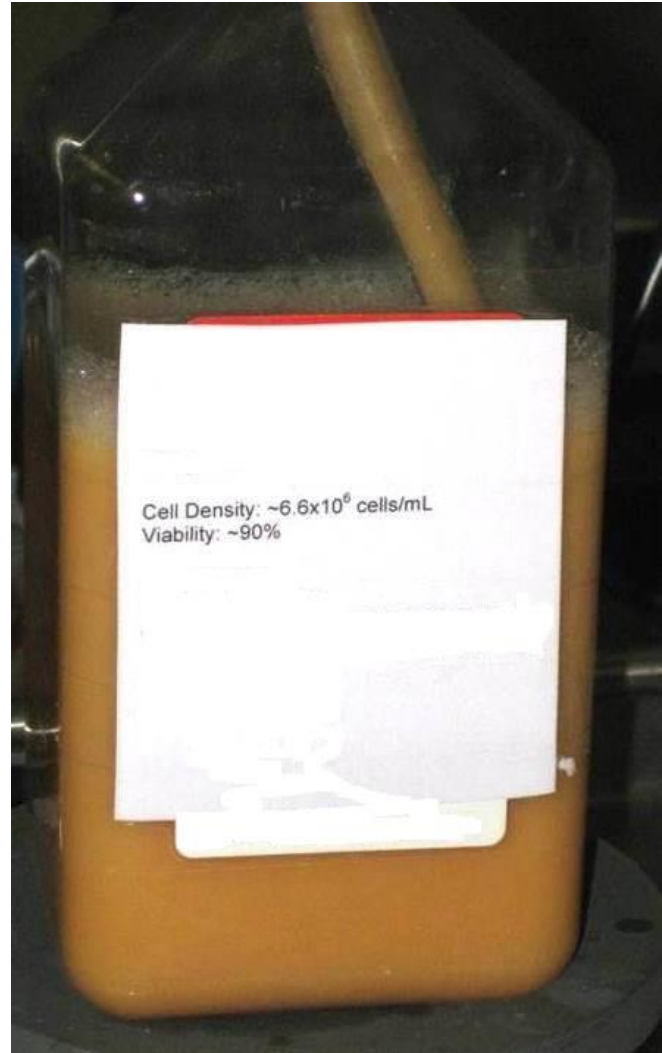
Diatomaceous earth = DE = Kieselguhr

- E. g. Celpure® (an imerys brand) → pharma grade
- Inorganic filter aid
- Mineralized organisms (skeleton of diatoms)

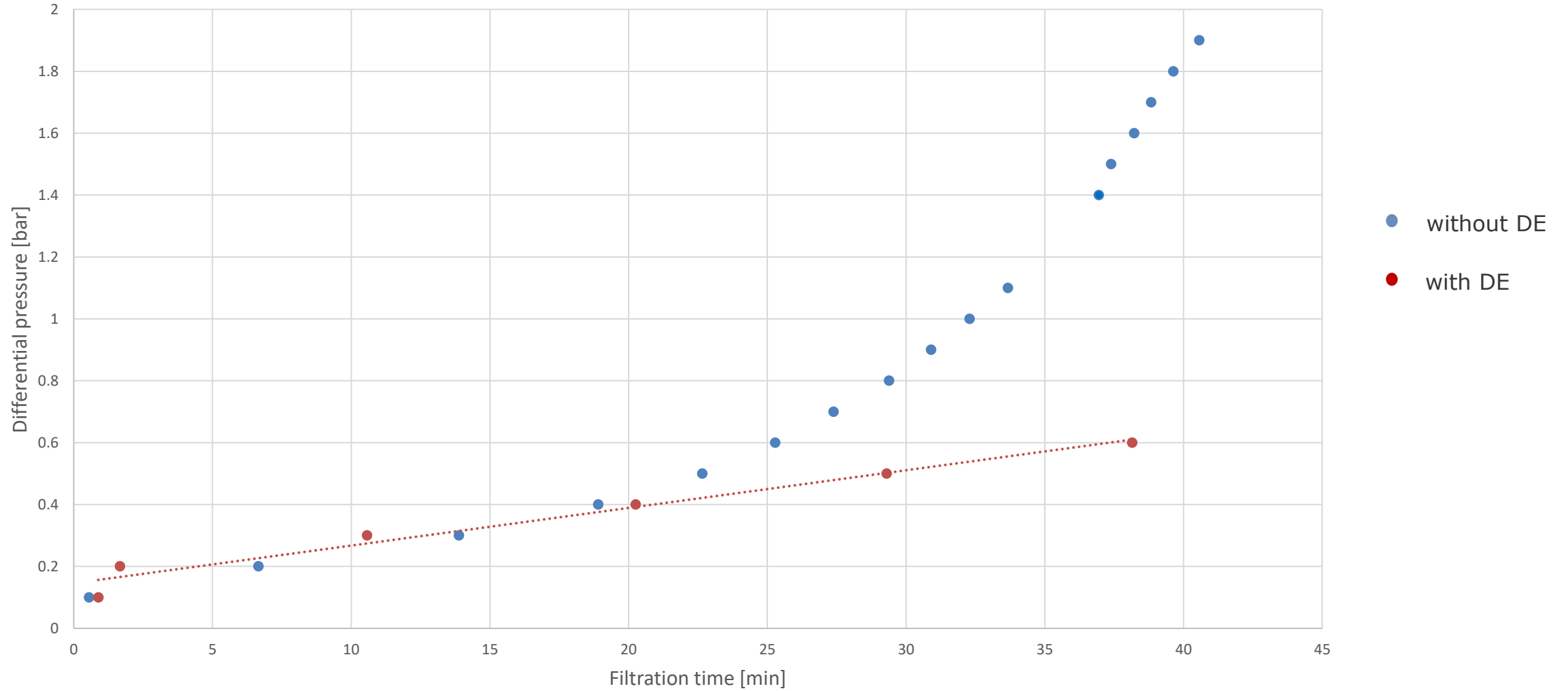
Grade	Permeability [mDarcy]	Solids removed* [µm]
C65	40 – 80	0.3 – 0.45
C100	70 – 140	0.3 – 0.45
C300	150 – 300	0.45 – 0.6
C1000	750 – 1250	> 1.0



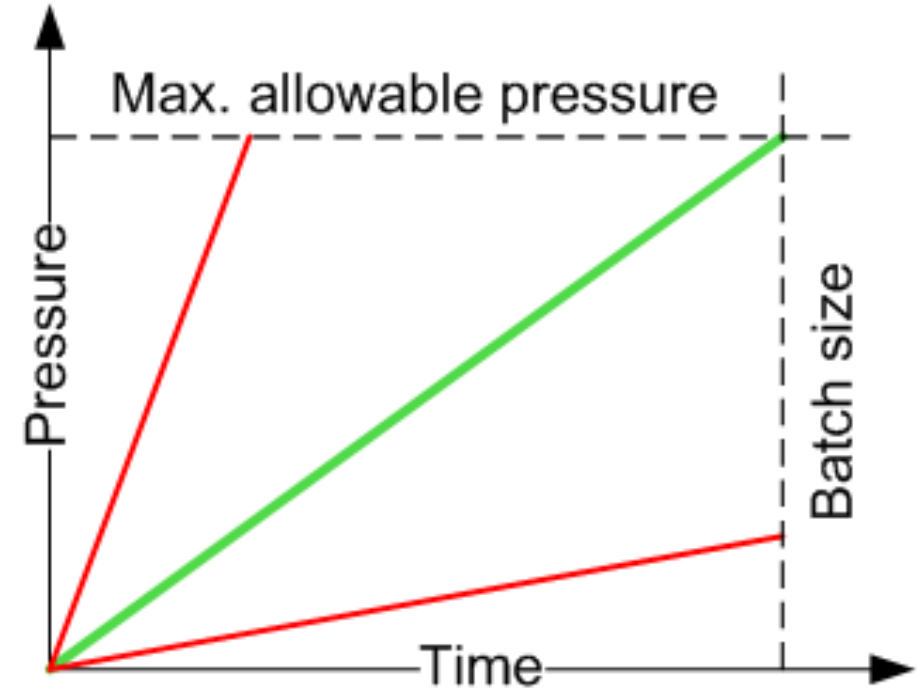
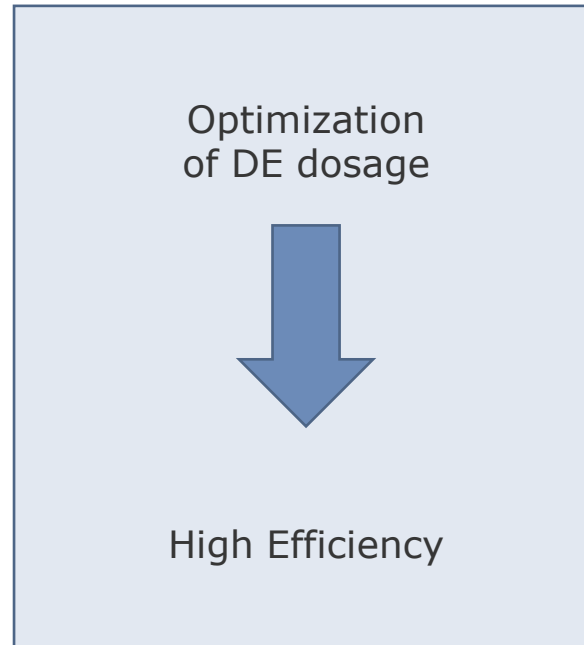
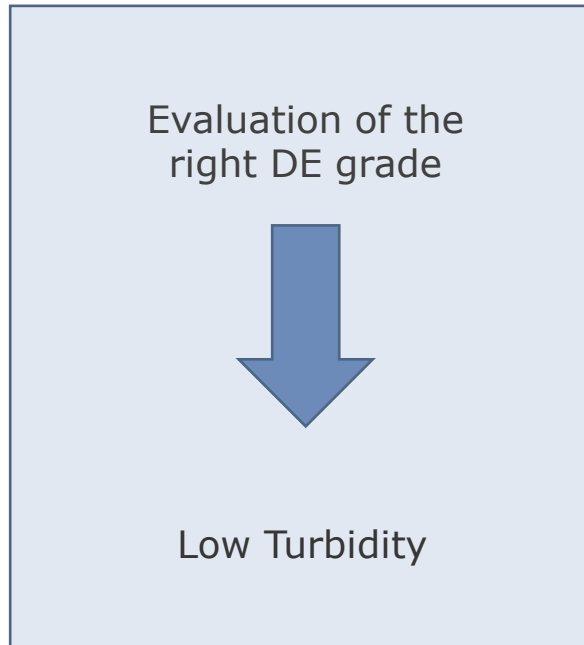
ALLUVIAL FILTRATION



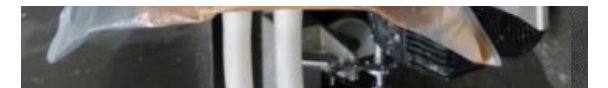
ALLUVIAL FILTRATION



FILTRODISC™ BIO SD



FILTRODISC™ BIO SD



AGENDA



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- Sheet vs. Depth vs. Alluvial filtration

Case Studies

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- 3) Depth Filtration vs. Alluvial filtration vs. pH adjustment
- 4) Influence of different filter sheet types
- 5) Scale up



CASE STUDIES

1

Mammalian cell
removal

2

Plasmid DNA
clarification

3

Depth filtration vs. DE
filtration vs. pH adjustment

4

Influence of different
filter sheet types

5

Scale up

1

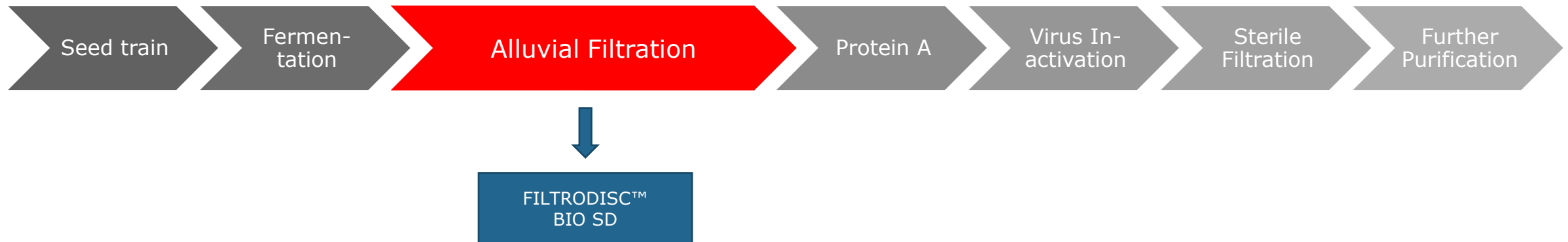
Case Studies

CASE STUDY: MAMMALIAN CELL REMOVAL



Background:

Typical clarification process for mammalian cells involves primary and secondary clarification step
→ Process step reduction with FILTRODISC™ BIO SD system and alluvial filtration technology



1

CASE STUDY: MAMMALIAN CELL REMOVAL



CHO cell culture producing IgG

- 2 days fed-batch cultivation
- 80 – 99 % viability
- $5 - 6 \times 10^6$ cells
- Harvest strategy:
 - FILTRODISC™ BIO SD 2"
 - PURAFIX® CH 09P
 - Comparison of Celpure® C100 and C300
 - Comparison of different Celpure® amounts
 - Filtration flux = $400 - 500 \text{ L/m}^2 \times \text{h}$

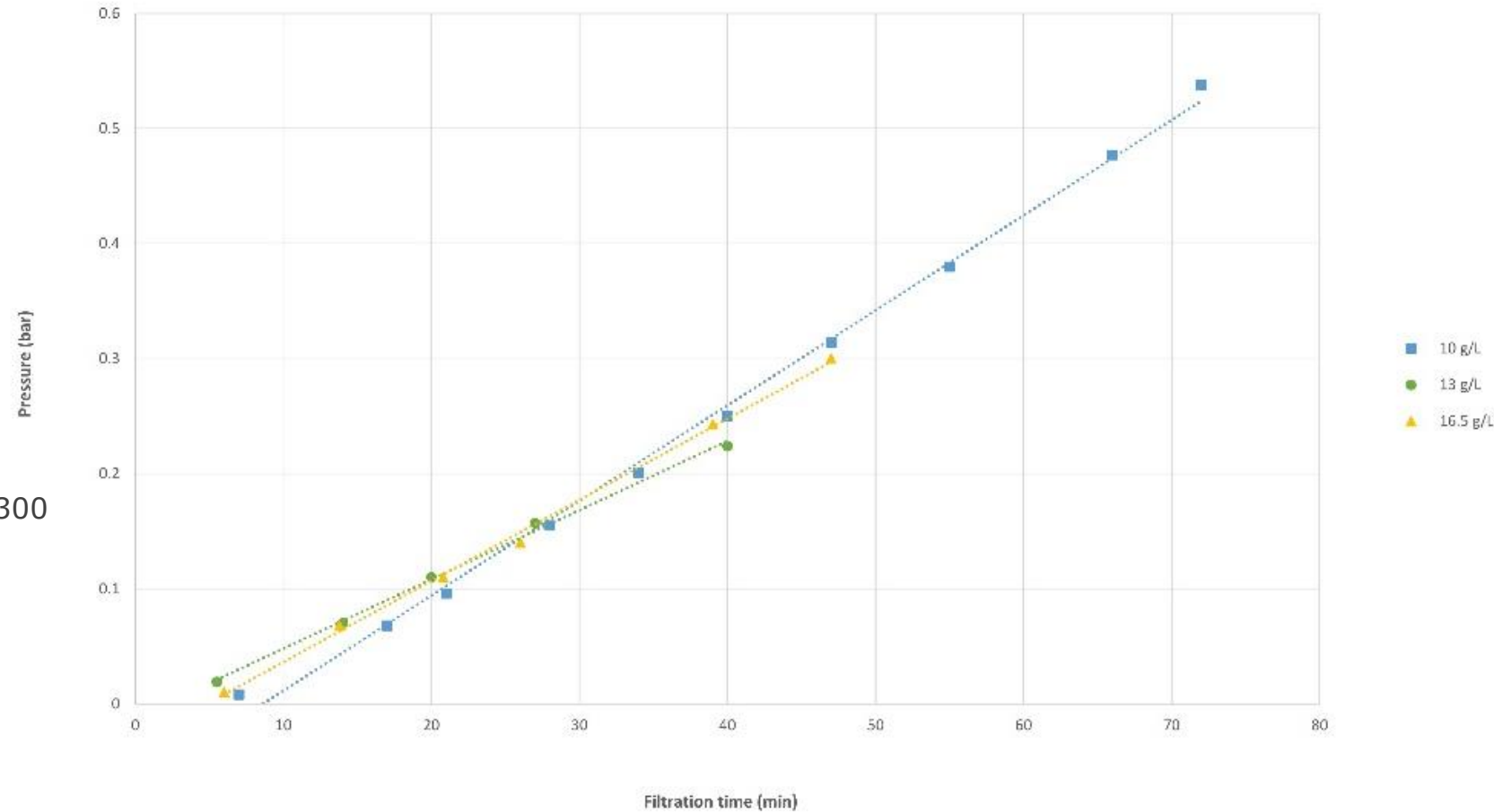


Figure: Pressure profiles as a function of throughput for different dosage of Celpure® 300

1

CASE STUDY: MAMMALIAN CELL REMOVAL

**CHO cell culture producing IgG**

→ Scale up from FILTRODISC™ BIO SD 2" to 5"

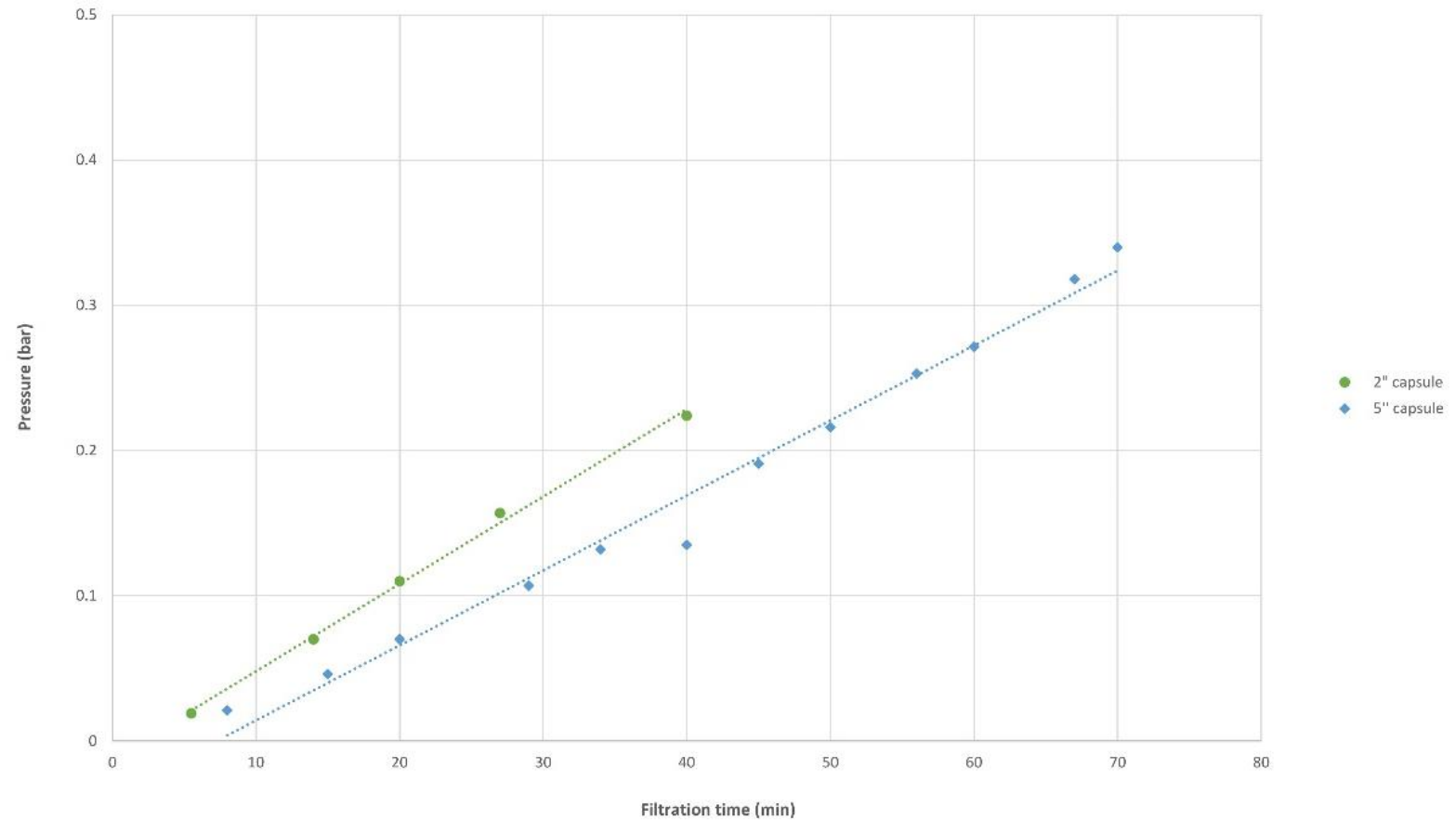


Figure: Pressure profiles (inlet) as a function of process time (throughput) for two different filtration FILTRODISC™ BIO SD 2" and 5" capsules and 13.5 g/L DE dose

1

CASE STUDY: MAMMALIAN CELL REMOVAL



CHO cell culture producing IgG
→ Recovery Yield

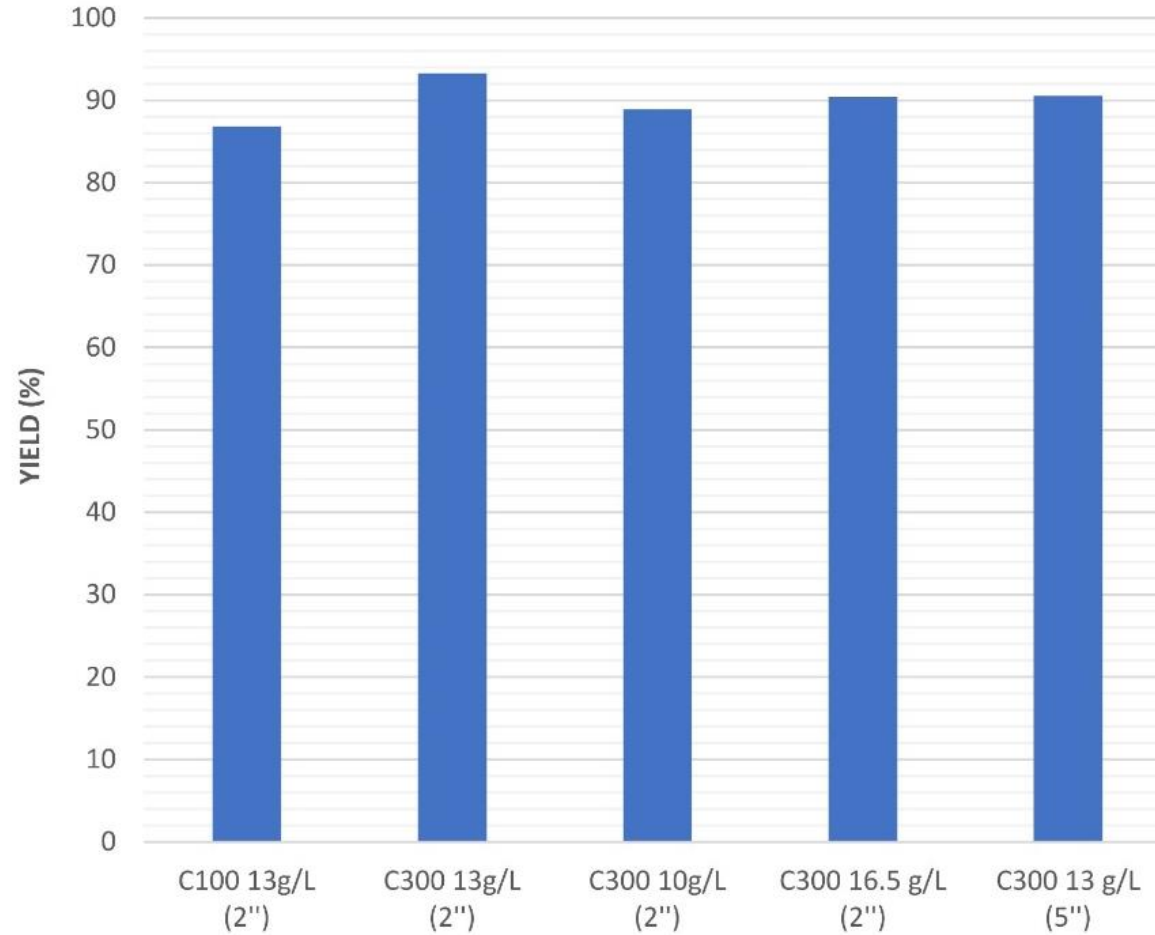


Figure: IgG recoveries in different filtration experiments

CASE STUDY: MAMMALIAN CELL REMOVAL



CHO cell culture producing IgG

→Results

- Productive approach
 - High flux (450 L/m²×h)
 - High throughput (400 L/m² as standard)
- Consistent clarification performance
 - Filtration fluxes
 - Throughputs
 - Reduction of turbidity
- Simple scale up
- Superior performance in terms of capacity & productivity (compared to alternative technologies)
- Cost efficiency → important for processes that are associated with “acceptance criteria” in terms of manufacturing costs

2

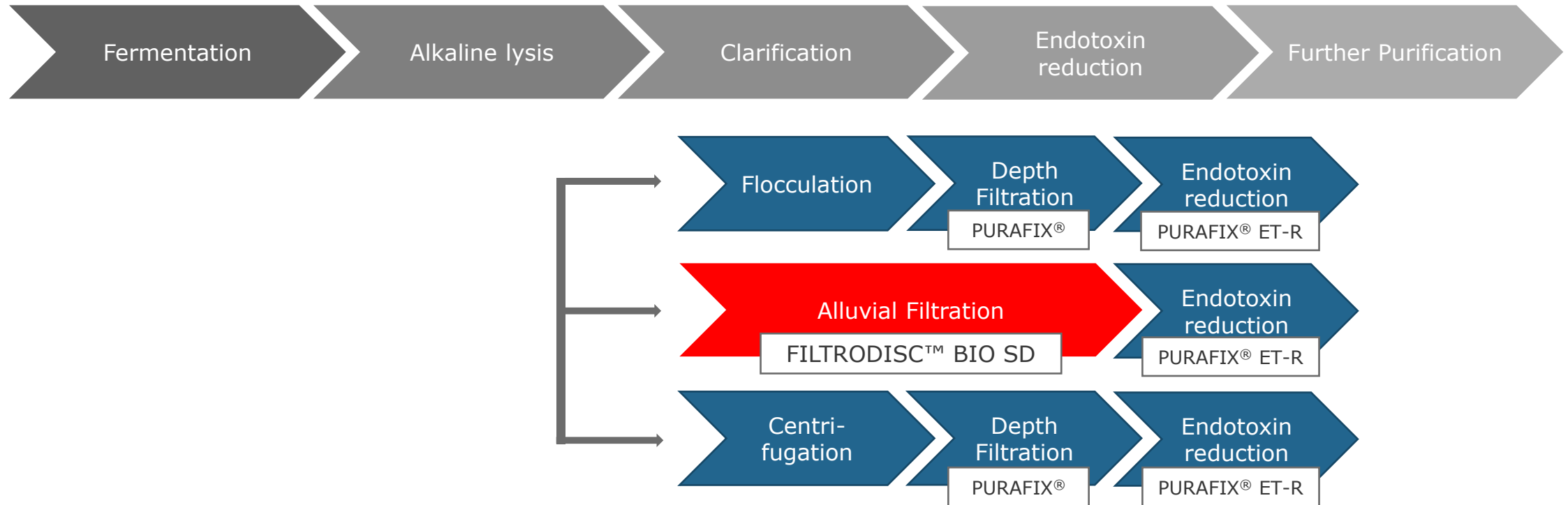
CASE STUDY: PLASMID DNA CLARIFICATION



Background:

Plasmid DNA is used in production of viral vectors.

→ Increasing demand for plasmid DNA leads to need for larger manufacturing capacities (due to increased clinical success and growing number of late-phase clinical studies)



2

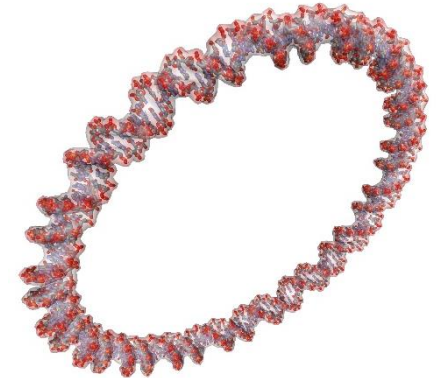
CASE STUDY: PLASMID DNA CLARIFICATION



Plasmid DNA production with FILTRODISC™ BIO SD and PURAFIX® ET-R

→Advantages

- Reduction of process steps (by elimination of centrifugation step)
- Process time reduction
- Cost effective reduction of impurities
- Flexible in terms of space for filter cake, retention rate, connectors etc.



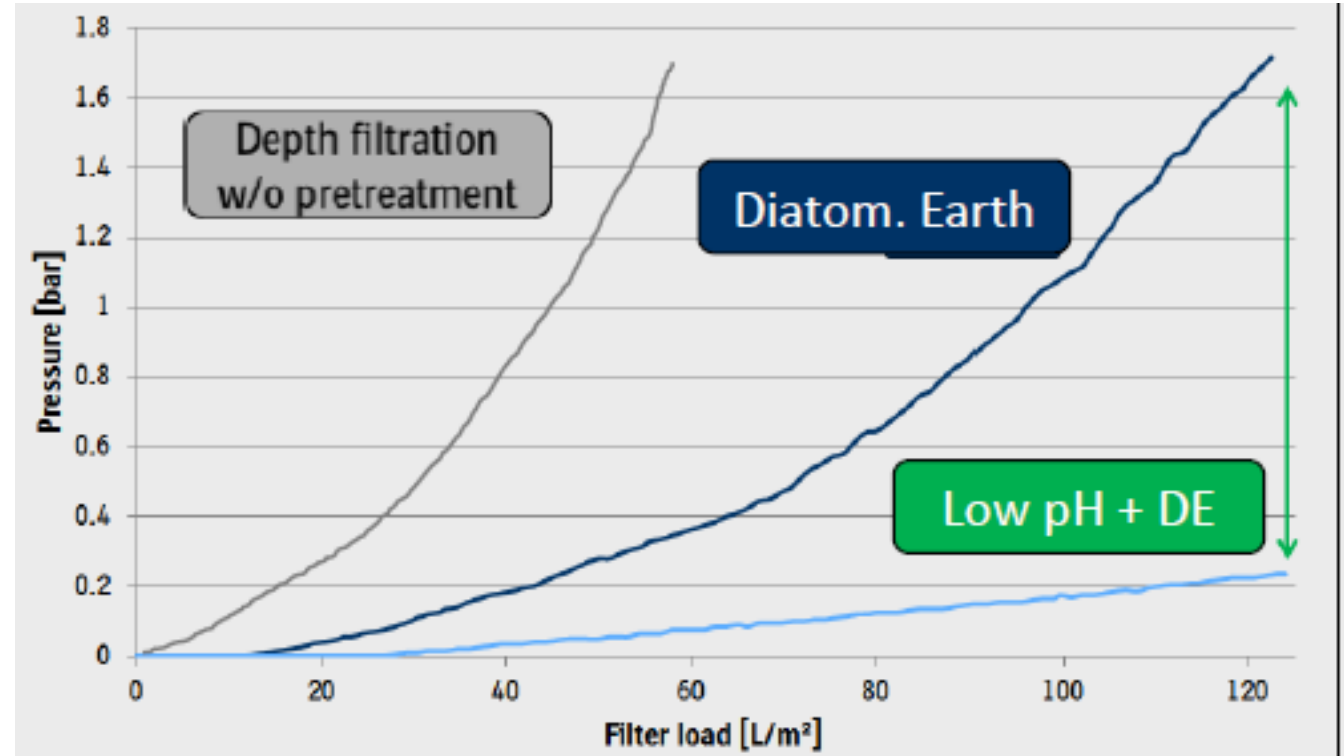
3

CASE STUDY: DEPTH FILTRATION VS. DE FILTRATION VS. ACID PRECIPITATION



Acid treatment / low pH:

- Leads to bigger particles
- Easier to filter
- Influence on target molecule?
- Afterwards pH needs to be adjusted again



Data published by Dr. Markus Brakel, Boehringer Ingelheim, BioProduction 2017 Dublin

4



CASE STUDY: INFLUENCE OF DIFFERENT DEPTH FILTER SHEET TYPES

Background: The use of filter sheets with different characteristics (retention rate) have an influence on the turbidity



Conditions:

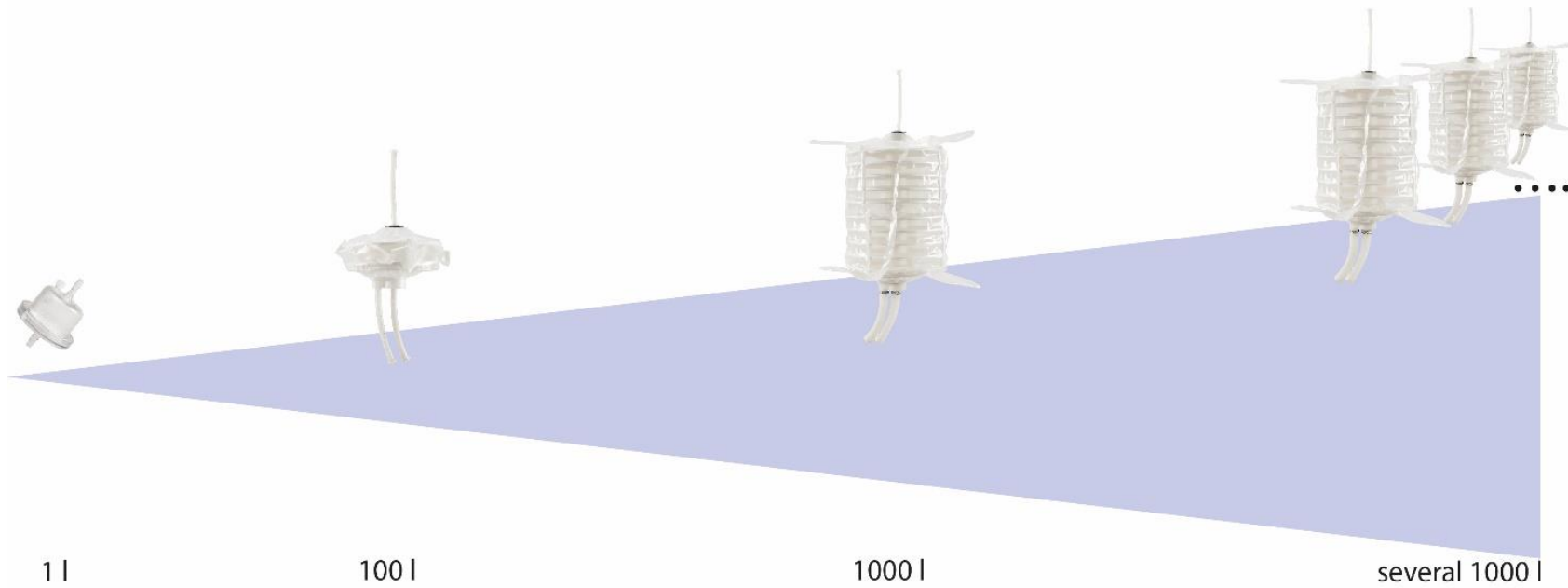
- 6×10^6 cells / mL
- Viability: 90 %
- Turbidity: 295 NTU
- DE grade: Celpure® C1000
- DE dosage: 25 g/L

	Trial 1	Trial 2
Filter sheet grade	PURAFIX® CH 9P	PURAFIX® CH ST 130P
Retention rate [µm]	30 – 10	0.6 – 0.4
Average flux [L/m²×h]	648	420
Turbidity after filtration [NTU]	3.8	1.5

5

Case Studies

CASE STUDY: SCALE UP



$$C_p = \frac{V_p \times C_L}{V_L}$$

$$C = h \times A$$

C: cake volume [m³]
 V: filtered volume [L]
 L: lab scale
 P: production scale
 h: cake height [m]
 A: filter area [m²]

5

CASE STUDY: SCALE UP

**Background:**

Laboratory scale filtration of a CHO cell culture

Conditions:

- FILTRODISC™ BIO SD 2" capsule (21 cm²)
- Filtered volume = 380 mL
- Final ΔP = 2.3 bar
- Filter aid type = Celpure® C300
- Filter aid dosage = 50 g/L
- Cake height = 3.0 cm
- Batch size = 100 L

**Scale up:**

$$A_{prod.}[m^2] = \frac{V_{prod.}[L] \times A_{test}[m^2]}{V_{test}[L]} = \frac{100 L \times 0.0021 m^2}{0.38 L} = 0.55 = 0.6 m^2$$

$$c_{prod.}[m^3] = \frac{V_{prod.}[L] \times c_{test}[m^3]}{V_{test}[L]} = \frac{100 L \times 0.000063 m^3}{0.38 L} = 0.0166 m^3 = 16.6 L$$

→ FILTRODISC™ BIO SD 12" double module

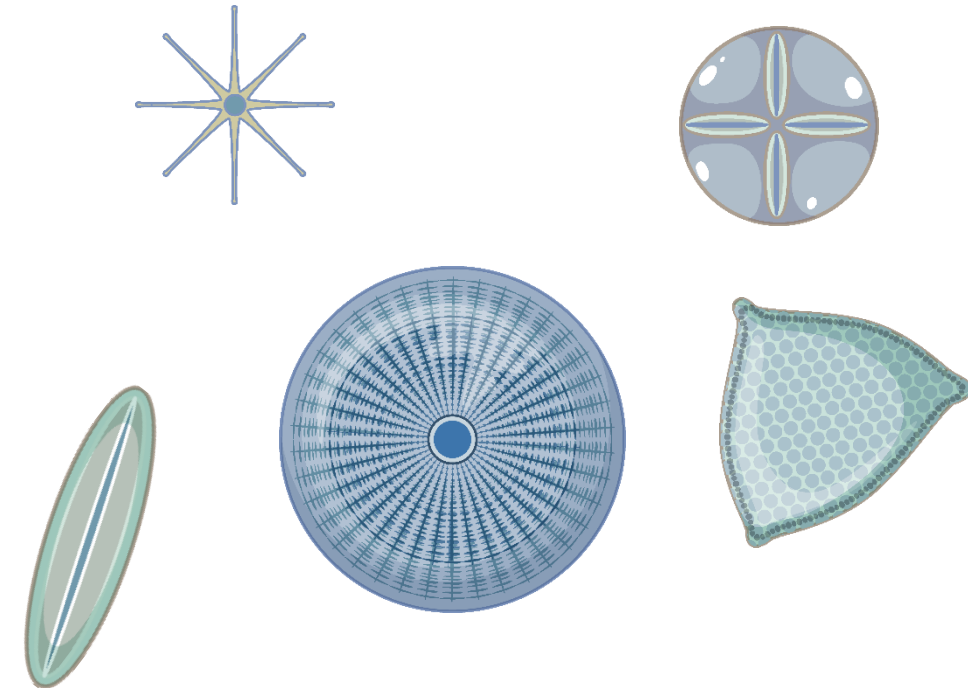
- 6 lenses per module (overall 12) = 1.32 m²
- Max holding volume = 17.8 L

TAKE-HOME MESSAGE



Advantages of Alluvial Filtration technology

- Well know and accepted technology (e. g. plasma fractionation)
- Removes cells and impurities in one step
- No need for pH changes or flocculants
- Reduce process time
- Different DE types available





SWISS QUALITY

DEPTH FILTRATION FOR VALUABLE LIQUIDS. SINCE 1938.

Let us solve your filtration task!

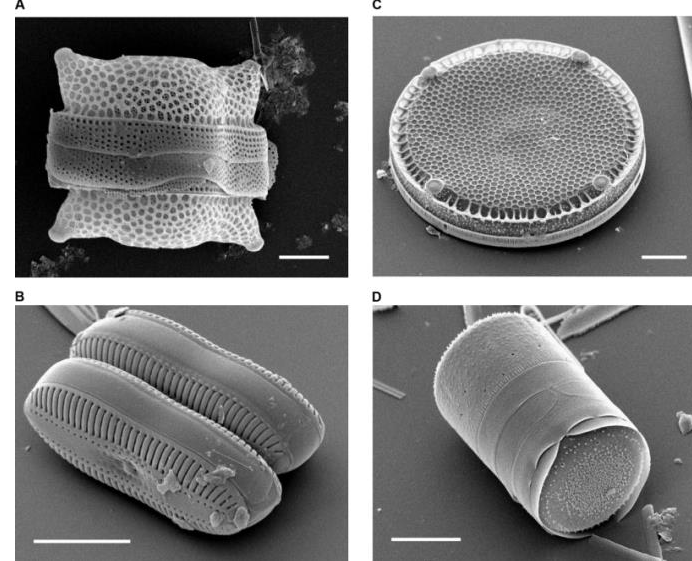
APPENDIX



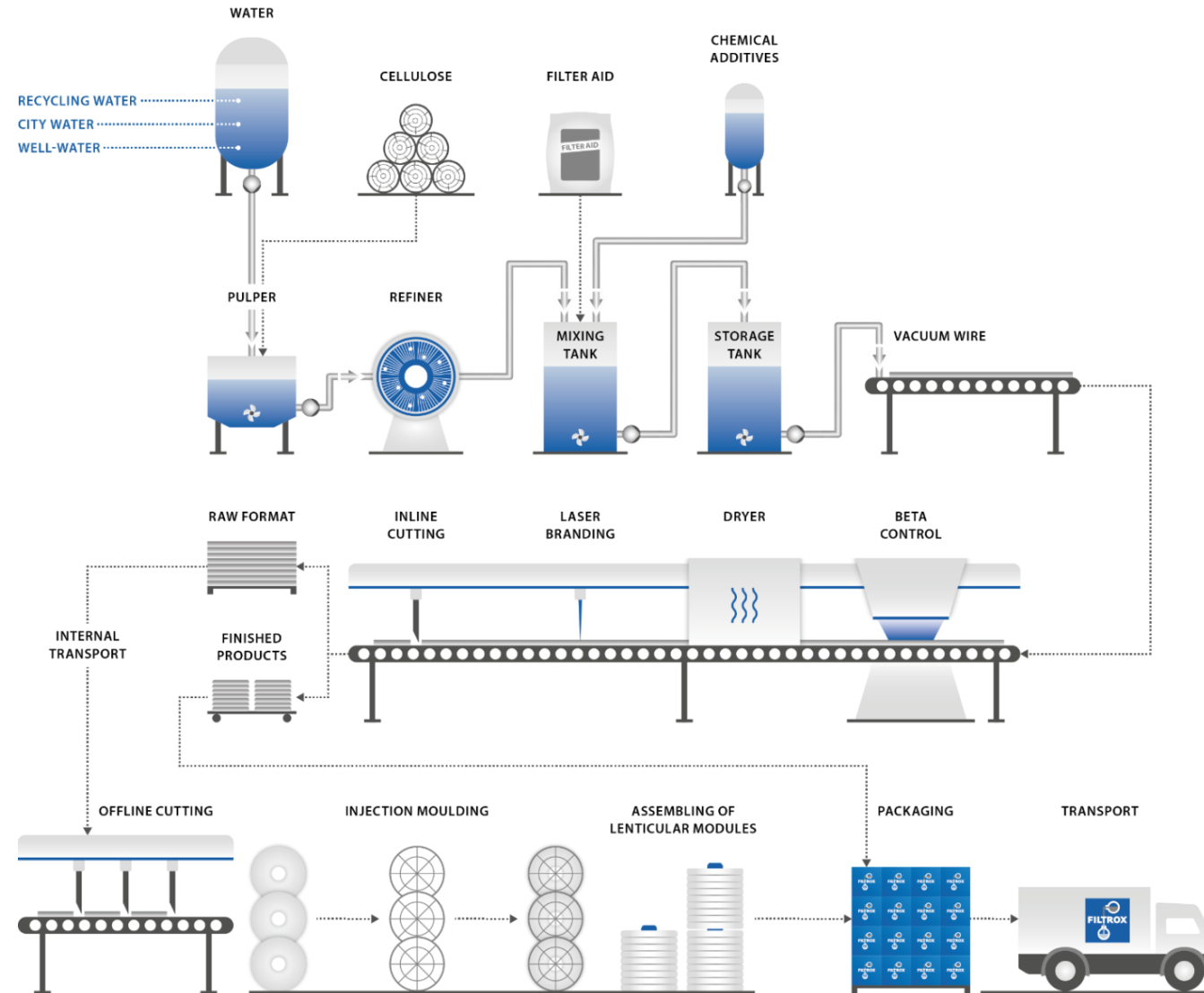
- Filter sheet composition
- Filter sheet production process
- Validation
- FILTRODISC™ BIO SD series
- FILTRODISC™ BIO SD: Filtration principle
- Laboratory scale set-up
- Powder Transfer
- Case Study: Viral Vector Clarification

FILTER SHEET COMPOSITION

- Cellulose fibers
 - Ground cellulose fibers form a 3D matrix
- Filter aid (e. g. Kieselguhr, Perlite)
 - Enlarge the inner surface
 - Improve the filtration effects
- Wet strength agent
 - Increase of wet tensile strength
 - Positive charge for the adsorption of negatively charged suspended solids



FILTER SHEET PRODUCTION PROCESS



PRIMARY PRODUCTION



Pulper



Wet sieve section



Drying Oven



Laser marking



SECONDARY PRODUCTION



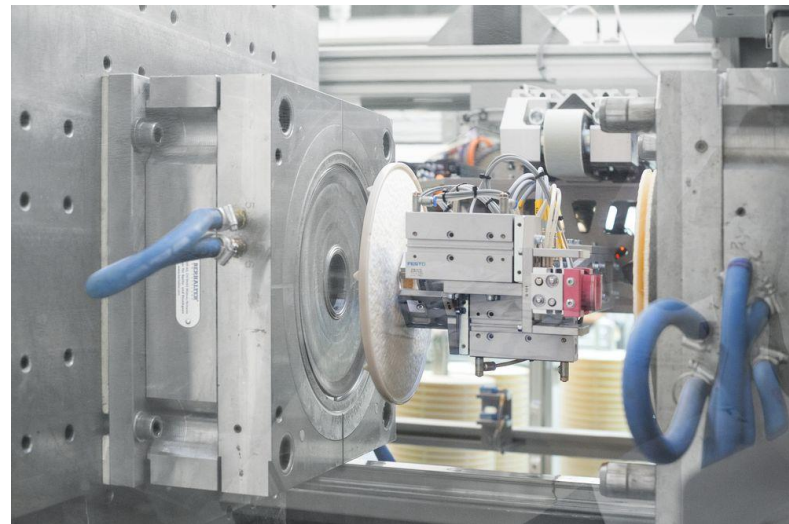
Stamping



Water jet



Modul-robot



Packaging

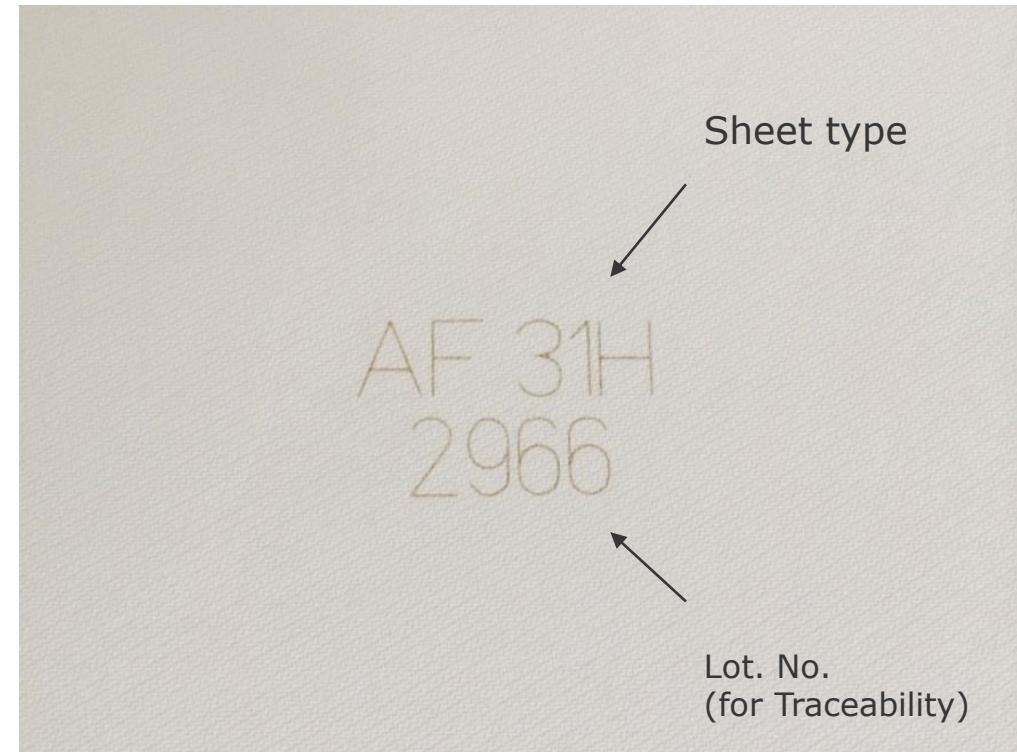


PRODUCTION PROCESS



Unfiltrat (coarse surface)

Filtrat (fine surface with laser marking)



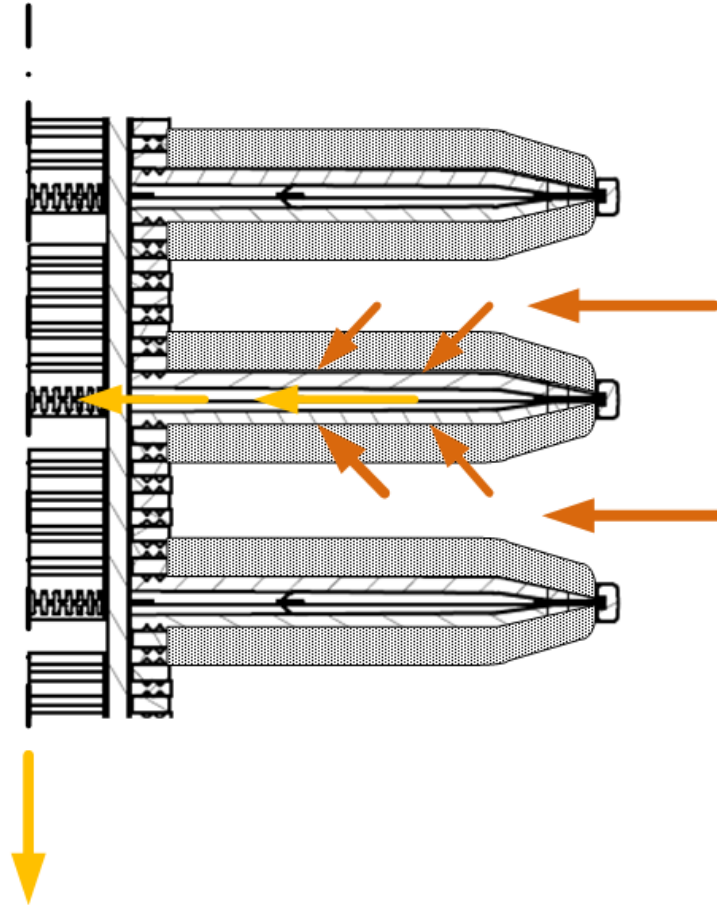
VALIDATION



Material of Construction

Supporting filter sheets:	PURAFIX® low ion and low pyrogen containing filter sheets
Filter aid:	Pharma grade Diatomaceous earth Celpure®; DE is already part of some sheet types
Bag material:	Double layer PE material, already used for other single-use applications (e. g. Bioreactors)
Tube:	APSH - Platinum Cured Silicone
Other plastic parts:	USP class VI material (e. g. core body and drainage nets of the modules)
Powder transfer bags:	LDPE with Permanent Anti-Static Additive

FILTRODISC™ BIO SD: FILTRATION PRINCIPLE



FILTRODISC™ BIO SD SERIES

2"



5"



10"



12"

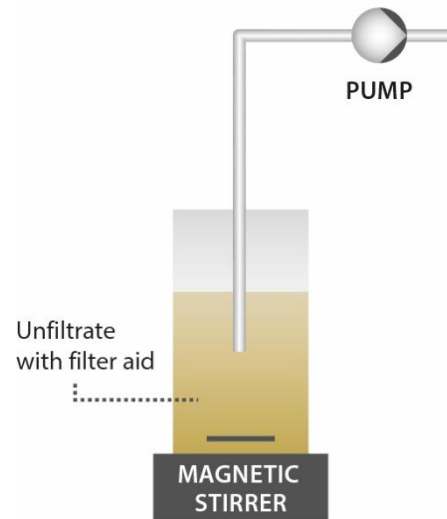


16"



LABORATORY SCALE SET-UP

Capsule test setup



Some important test parameters:

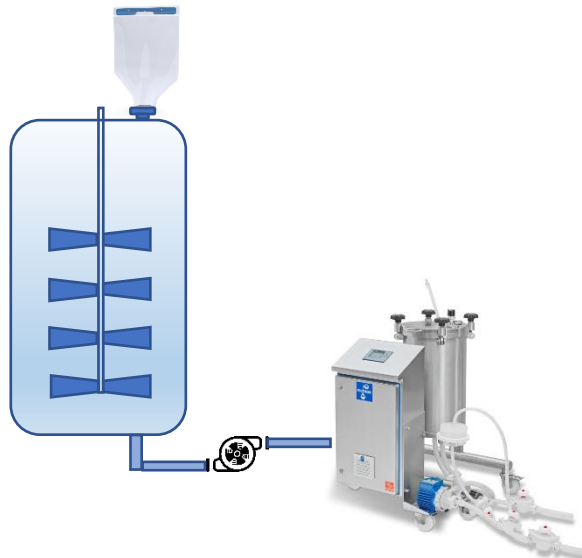
- Pump need to keep the flow even with increasing pressure
- Tube connection as short as possible
- Follow the instruction in the handbook or in the playbook alluvial filtration

POWDER TRANSFER

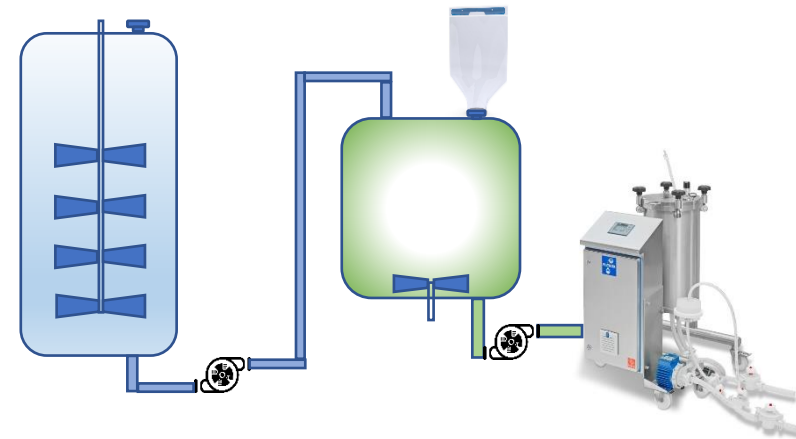
Powder Transfer into the Process

Direct mixing with fermentation broth / cell homogenate

1. Feeding filter aid into bioreactor
(only if single-use bioreactor)



2. Transfer fermentation broth into mixing unit and feeding filter aid

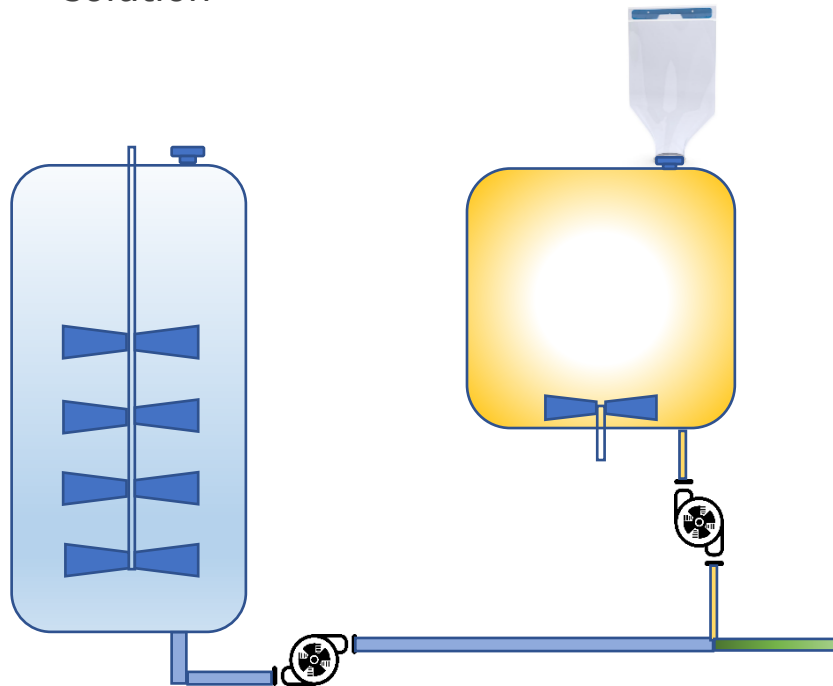


POWDER TRANSFER

Powder Transfer into the Process

Direct mixing with fermentation broth / cell homogenate

3. Body feed with a pre-prepared slurry solution



Mixing buffer with filter aid in a single-use mixer and add the solution into the line to the filter

CASE STUDY: VIRAL VECTOR CLARIFICATION

Background:

Adeno-associated viruses (AAV) and lentiviruses are currently being developed for numerous indications in field of gene therapy.

→ First step in both direct and cell-based gene therapy = packaging a therapeutic transgene into a delivery vehicle (e. g. a viral vector), followed by expansion of host cell lines to produce high-enough vector concentrations

